1.B.2.c - Venting and Flaring

Category Code	Method				AD				EF						
1.B.2.c	T2			AS				CS							
Key Category	SO2	NO×	NH₃	NMVOC	СО	BC	Pb	Hg	Cd	Diox	PAH	HCB	TSP	PM 10	PM2 5
1.B.2.c	-/-	-/-	-	-/-	-/-	-/-	-	-/-	-	-	-	-	-/-	-/-	-/-

T =	key source by Trend $\mathbf{L} = \mathbf{k}$	ey source l	by Level						
Me	ethods								
	D	Defa	ult						
	T1	Tier	1 / Simple Methodology *						
	T2	Tier	2*						
	Т3	Tier	3 / Detailed Methodology *						
	С	COR	INAIR						
CS C		Coui	Country Specific						
	М	Mod							
			Inventory Guidebook - 2019, in the group specific chapters.						
AD	- Data Source for Activi	ty Data							
NS	National Statistics								
RS	Regional Statistics								
IS	International Statistics								
	Plant Specific data								
As	Associations, business orga	anisations							
	specific Questionnaires (or	surveys)							
	Model / Modelled								
С	Confidential								
EF	- Emission Factors								
D	Default (EMEP Guidebook)								
С	Confidential								
CS	Country Specific								
PS	Plant Specific data								
Μ	Model / Modelled								

Pursuant to general requirements of the Technical Instructions on Air Quality Control TA Luft (2002), gases, steam, hydrogen and hydrogen sulphide released from pressure valves and venting equipment must be collected in a gas-collection system. Wherever possible, gases so collected are burned in process combustion. Where such use is not possible, the gases are piped to a flare. Flares used for flaring of such gases must fulfill at least the requirements for flares for combustion of gases from operational disruptions and from safety valves. For refineries and other types of plants in categories 1.B.2, flares are indispensable safety components. In crude-oil refining, excessive pressures can build up in process systems, for various reasons. Such excessive pressures have to be reduced via safety valves, to prevent tanks and pipelines from bursting. Safety valves release relevant products into pipelines that lead to flares. Flares carry out controlled burning of gases released via excessive pressures. When in place, flare-gas recovery systems liquify the majority of such gases and return them to refining processes or to refinery combustion systems. In the process, more than 99 % of the hydrocarbons in the gases are converted to CO₂ and H₂O. When a plant has such systems in operation, its flarehead will seldom show more than a small pilot flame.

	Unit	1990	1995	2000	2005	2010	2015	2018	2019
Flared natural gas	millions of m ³	36	33	36	18.7	12.1	10.5	10.6	15.6
Refined crude-oil quantity	millions of t	107	96.5	107.6	114.6	95.4	93.4	87.7	87

Flaring takes place in extraction and pumping systems and at refineries. In refineries, flaring operations are subdivided into regular operations and start-up / shut-down operations in connection with disruptions.

Source of emission factor	Substance Unit			ľ	Value			
Flaring emissions in natural gas extraction	NMVOC	k	kg/ 1000 m ³		0.005			
Flaring emissions in natural gas extraction	NO×	(g/ 1000 m ³		1.269				
Flaring emissions in natural gas extraction	SO2	g/ 1000	g/ 1000 m³					
Flaring emissions in natural gas extraction	CO	k	g/ 1000) m³	0.726			
Source of emission factor		Sub	stance	Unit	Value			
Flaring emissions at petroleum production	facilities	NO×		kg/t	0.008			
Flaring emissions at petroleum production	SO2		kg/t	0.010				
Flaring emissions at petroleum production	facilities	CO		g/t	0.1			
Source of emission factor			Subst	ance	Unit	Valu	e	
Flaring emissions at refineries: normal flari	tions	NMV	OC	kg/m³	0.00)4		
Flaring emissions at refineries: normal flari	ng opera	tions	CO kg/m		kg/m³	0.00)1	
Flaring emissions at refineries: normal flari	ng opera	tions	5 SO2		kg/m³	0.00)3	
Flaring emissions at refineries: normal flari	ng opera	tions	NC	NO _× g/m		0.4		
Source of emission factor		Subs	stance	Unit	Valu	e		
Flaring emissions at refineries: disruptions	rations	NMV	OC	kg/t	0.00	1		
Flaring emissions at refineries: disruptions	CO		kg/t	0.00	1			
Flaring emissions at refineries: disruptions	SO ₂		kg/t	0.00	7			
Flaring emissions at refineries: disruptions	NO×		kg/t	0.00	4			

The emission factors have been derived from the 2004 and 2008 emissions declarations Theloke et al. 2013 ¹⁾. In 2019, they were updated for CH₄, N₂O, CO, NMVOC, NO_x and SO₂, on the basis of Bender & von Müller, 2019 ²⁾. Venting emissions are taken into account in category 1.B.2.b.iii. The SO₂ emissions are obtained from the activity data for the flared natural gas (Table 178) and an emission factor of 0.140 kg / 1,000 m³, a factor which takes account of an average H₂S content of 5 % by volume. The emission factors are determined on the basis of emissions reports, crude-oil-refining capacity and total capacity utilisation at German refineries. The guide for this work consists of the evaluation assessment of Theloke et al. (2013) ³⁾.

Recalculations

will be published later - in meantime please refer to chapter 8.1 "recalculations"

Planned improvements

Currently no improvements are planned.

References

^{1). 3)} Theloke, J., Kampffmeyer, T., Kugler, U., Friedrich, R., Schilling, S., Wolf, L., & Springwald, T. (2013). Ermittlung von Emissionsfaktoren und Aktivitätsraten im Bereich IPCC (1996) 1.B.2.a. i-vi - Diffuse Emissionen aus Mineralöl und Mineralölprodukten (Förderkennzeichen 360 16 033). Stuttgart.

²⁾ Bender, M., & von Müller, G. (2019). Konsolidierung der Treibhausgasemissionsberechnungen unter der 2. Verpflichtungsperiode des Kyoto-Protokolls und der neuen Klimaschutz-Berichterstattungs-pflichten an die EU (FKZ 3716 41 107 0).