1.B.2.c - Venting and Flaring

Category Code	Method				AD				EF						
1.B.2.c	T2				AS				CS						
Key Category	NOx	NMVOC	SO ₂	NH₃	PM _{2.5}	\mathbf{PM}_{10}	TSP	BC	СО	PB	Cd	Hg	Diox	PAH	нсв
1.B.2.c	-/-	-/-	-/-	-	-/-	-/-	-/-	-/-	-/-	-	-	-/-	-	-	-

т -	• key source by Trend L = k	av source l	
		ey source i	
Me	ethods		
	D	Defa	-
	T1		1 / Simple Methodology *
	T2	Tier	
	Т3		3 / Detailed Methodology *
	С	COR	INAIR
	CS	Cour	ntry Specific
	Μ	Mod	el
* a	s described in the EMEP/EE	A Emission	Inventory Guidebook - 2019, in the group specific chapters.
AD	- Data Source for Activi	ty Data	
NS	National Statistics		
RS	Regional Statistics		
IS	International Statistics		
PS	Plant Specific data		
As	Associations, business org	anisations	
Q	specific Questionnaires (or	surveys)	
М	Model / Modelled		
С	Confidential		
EF	- Emission Factors		
D	Default (EMEP Guidebook)		
	Confidential		
CS	Country Specific		
<u> </u>	Plant Specific data		
<u> </u>	Model / Modelled		

Pursuant to general requirements of the Technical Instructions on Air Quality Control TA Luft (2002), gases, steam, hydrogen and hydrogen sulphide released from pressure valves and venting equipment must be collected in a gas-collection system. Wherever possible, gases so collected are burned in process combustion. Where such use is not possible, the gases are piped to a flare. Flares used for flaring of such gases must fulfill at least the requirements for flares for combustion of gases from operational disruptions and from safety valves. For refineries and other types of plants in categories 1.B.2, flares are indispensable safety components. In crude-oil refining, excessive pressures can build up in process systems, for various reasons. Such excessive pressures have to be reduced via safety valves, to prevent tanks and pipelines from bursting. Safety valves release relevant products into pipelines that lead to flares. Flares carry out controlled burning of gases released via excessive pressures. When in place, flare-gas recovery systems liquify the majority of such gases and return them to refining processes or to refinery combustion systems. In the process, more than 99 % of the hydrocarbons in the gases are converted to CO₂ and H₂O. When a plant has such systems in operation, its flarehead will seldom show more than a small pilot flame.

Table 1: Activity data applied for 1.B.2.c

	Unit	1990	1995	2000	2005	2010	2015	2020	2021
Flared natural gas	millions of m ³	36	33	36	18.7	12.1	10.5	14.1	11.1
Refined crude-oil quantity	millions of t	107	96.5	107.6	114.6	95.4	93.4	84.0	84.1

Flaring takes place in extraction and pumping systems and at refineries. In refineries, flaring operations are subdivided into regular operations and start-up / shut-down operations in connection with disruptions.

Table 2: Emission factors applied for flaring emissions in natural gas extraction, in [kg/ 1000 m³]

Source of emission factor	Substar	nce l	Jnit		Value			
laring emissions in natural gas extraction NMVOC			cg/ 100)0 m³	0.005			
Flaring emissions in natural gas extraction	k	(g/ 100)0 m³	1.269				
Flaring emissions in natural gas extraction	ring emissions in natural gas extraction SO2)0 m³	8.885			
Flaring emissions in natural gas extraction	laring emissions in natural gas extraction CO				0.726	_		
Source of emission factor	Sub	stanc	e Uni	t Value				
Flaring emissions at petroleum production	NO×		kg/t 0.00					
Flaring emissions at petroleum production	SO2		kg/t 0.010					
Flaring emissions at petroleum production	CO		g/t	0.1				
Source of emission factor			Subs	tance	e Unit	Valu	е	
Flaring emissions at refineries: normal flaring opera			5 NM	VOC	/OC kg/m ³		4	
Flaring emissions at refineries: normal flari	itions	6 (0	kg/m³	0.00	1		
Flaring emissions at refineries: normal flaring operati				02	kg/m³	0.00	3	
Flaring emissions at refineries: normal flaring operations					g/m³	0.4		
Source of emission factor	Sub	stance	Unit	Va	lue			
Flaring emissions at refineries: disruptions of flaring operations					NMVOC		0.0	01
Flaring emissions at refineries: disruptions	s CO	СО		0.0	01			
Flaring emissions at refineries: disruptions	s SO2	SO2		0.0	07			
Flaring emissions at refineries: disruptions	s NO _×		kg/t	0.0	04			

The emission factors have been derived from the 2004 and 2008 emissions declarations Theloke et al. 2013 ¹⁾. In 2019, they were updated for CH₄, N₂O, CO, NMVOC, NO_x and SO₂, on the basis of Bender & von Müller, 2019 ²⁾. Venting emissions are taken into account in category 1.B.2.b.iii. The SO₂ emissions are obtained from the activity data for the flared natural gas (Table 178) and an emission factor of 0.140 kg / 1,000 m³, a factor which takes account of an average H₂S content of 5 % by volume. The emission factors are determined on the basis of emissions reports, crude-oil-refining capacity and total capacity utilisation at German refineries. The guide for this work consists of the evaluation assessment of Theloke et al. (2013) ³.

Recalculations

Please refer to overarching chapter 1.B - Fugitive Emissions from fossil fuels

Planned improvements

Currently no improvements are planned.

References

²⁾ Bender, M., & von Müller, G. (2019). Konsolidierung der Treibhausgasemissionsberechnungen unter der 2. Verpflichtungsperiode des Kyoto-Protokolls und der neuen Klimaschutz-Berichterstattungs-pflichten an die EU (FKZ 3716 41 107 0).

^{1), 3)} Theloke, J., Kampffmeyer, T., Kugler, U., Friedrich, R., Schilling, S., Wolf, L., & Springwald, T. (2013). Ermittlung von Emissionsfaktoren und Aktivitätsraten im Bereich IPCC (1996) 1.B.2.a. i-vi - Diffuse Emissionen aus Mineralöl und Mineralölprodukten (Förderkennzeichen 360 16 033). Stuttgart.