

## 1.B.2.c - Venting and Flaring

Category Code	Method					AD					EF				
1.B.2.c	T2					AS					CS				
Key Category	NO <sub>x</sub>	NM VOC	SO <sub>2</sub>	NH <sub>3</sub>	PM <sub>2.5</sub>	PM <sub>10</sub>	TSP	BC	CO	PB	Cd	Hg	Diox	PAH	HCB
1.B.2.c	-/-	-/-	-/-	-	-/-	-/-	-/-	-/-	-/-	-	-	-/-	-	-	-

Method(s) applied	
<b>D</b>	Default
<b>T1</b>	Tier 1 / Simple Methodology *
<b>T2</b>	Tier 2*
<b>T3</b>	Tier 3 / Detailed Methodology *
<b>C</b>	CORINAIR
<b>CS</b>	Country Specific
<b>M</b>	Model
* as described in the EMEP/EEA Emission Inventory Guidebook - 2019, in category chapters.	
(source for) Activity Data	
<b>NS</b>	National Statistics
<b>RS</b>	Regional Statistics
<b>IS</b>	International Statistics
<b>PS</b>	Plant Specific
<b>As</b>	Associations, business organisations
<b>Q</b>	specific Questionnaires (or surveys)
<b>M</b>	Model / Modelled
<b>C</b>	Confidential
(source for) Emission Factors	
<b>D</b>	Default (EMEP Guidebook)
<b>CS</b>	Country Specific
<b>PS</b>	Plant Specific
<b>M</b>	Model / Modelled
<b>C</b>	Confidential

Pursuant to general requirements of the Technical Instructions on Air Quality Control TA Luft (2002), gases, steam, hydrogen and hydrogen sulphide released from pressure valves and venting equipment must be collected in a gas-collection system. Wherever possible, gases so collected are burned in process combustion. Where such use is not possible, the gases are piped to a flare. Flares used for flaring of such gases must fulfill at least the requirements for flares for combustion of gases from operational disruptions and from safety valves. For refineries and other types of plants in categories 1.B.2, flares are indispensable safety components. In crude-oil refining, excessive pressures can build up in process systems, for various reasons.

Such excessive pressures have to be reduced via safety valves, to prevent tanks and pipelines from bursting. Safety valves release relevant products into pipelines that lead to flares. Flares carry out controlled burning of gases released via excessive pressures. When in place, flare-gas recovery systems liquify the majority of such gases and return them to refining processes or to refinery combustion systems. In the process, more than 99 % of the hydrocarbons in the gases are converted to CO<sub>2</sub> and H<sub>2</sub>O. When a plant has such systems in operation, its flarehead will seldom show more than a small pilot flame.

Table 1: Activity data applied for 1.B.2.c

	Unit	1990	1995	2000	2005	2010	2015	2020	2021
Flared natural gas	millions of m <sup>3</sup>	36	33	36	18.7	12.1	10.5	14.1	11.1
Refined crude-oil quantity	millions of t	107	96.5	107.6	114.6	95.4	93.4	84.0	84.1

Flaring takes place in extraction and pumping systems and at refineries. In refineries, flaring operations are subdivided into

regular operations and start-up / shut-down operations in connection with disruptions.

Table 2: Emission factors applied for flaring emissions in natural gas extraction, in [kg/ 1000 m<sup>3</sup>]

	Value
<b>NM VOC</b>	0.005
<b>NO<sub>x</sub></b>	1.269
<b>SO<sub>2</sub></b>	8.885
<b>CO</b>	0.726

Table 3: Emission factors applied for flaring emissions at petroleum production facilities

	Unit	Value
<b>NO<sub>x</sub></b>	kg/t	0.008
<b>SO<sub>2</sub></b>	kg/t	0.010
<b>CO</b>	g/t	0.1

Table 4: Emission factors applied for flaring emissions at refineries: normal flaring operations

	Unit	Value
<b>NM VOC</b>	kg/m <sup>3</sup>	0.004
<b>CO</b>	kg/m <sup>3</sup>	0.001
<b>SO<sub>2</sub></b>	kg/m <sup>3</sup>	0.003
<b>NO<sub>x</sub></b>	g/m <sup>3</sup>	0.4

Table 5: Emission factors applied for flaring emissions at refineries: disruptions of flaring operations, in [kg/t]

	Value
<b>NM VOC</b>	0.001
<b>CO</b>	0.001
<b>SO<sub>2</sub></b>	0.007
<b>NO<sub>x</sub></b>	0.004

The emission factors have been derived from the 2004 and 2008 emissions declarations Theloke et al. 2013 <sup>1)</sup>. In 2019, they were updated for CH<sub>4</sub>, N<sub>2</sub>O, CO, NM VOC, NO<sub>x</sub> and SO<sub>2</sub>, on the basis of Bender & von Müller, 2019 <sup>2)</sup>.

Venting emissions are taken into account in category 1.B.2.b.iii. The SO<sub>2</sub> emissions are obtained from the activity data for the flared natural gas (Table 178) and an emission factor of 0.140 kg / 1,000 m<sup>3</sup>, a factor which takes account of an average H<sub>2</sub>S content of 5 % by volume. The emission factors are determined on the basis of emissions reports, crude-oil-refining capacity and total capacity utilisation at German refineries. The guide for this work consists of the evaluation assessment of Theloke et al. (2013) <sup>3)</sup>.

## Recalculations



For more details please refer to the super-ordinate chapter [1.B - Fugitive Emissions from fossil fuels](#)

## Planned improvements

Currently no improvements are planned.

## References

---

<sup>1), 3)</sup> Theloke, J., Kampffmeyer, T., Kugler, U., Friedrich, R., Schilling, S., Wolf, L., & Springwald, T. (2013). Ermittlung von Emissionsfaktoren und Aktivitätsraten im Bereich IPCC (1996) 1.B.2.a. i-vi - Diffuse Emissionen aus Mineralöl und Mineralölprodukten (Förderkennzeichen 360 16 033). Stuttgart.

<sup>2)</sup> Bender, M., & von Müller, G. (2019). Konsolidierung der Treibhausgasemissionsberechnungen unter der 2. Verpflichtungsperiode des Kyoto-Protokolls und der neuen Klimaschutz-Berichterstattungs-pflichten an die EU (FKZ 3716 41 107 0).